

PROCESS DATA SHEET FOR HDS REACTOR HEATER
(H-8201) OF RFCC NAPHTHA TREATING UNIT

UNIT	Type of Heater	Cylindrical		Manufacturer		Rev
2	Total Heater Absorbed Duty, MW	11.03 (13)				
3	PROCESS DESIGN CONDITIONS					
4	Operating Case	10 PPM EOR		50 PPM SOR Turndown		Regeneration
5	Heater Section	Radiant & Conv.		Radiant & Conv.		Radiant & Conv.
6	Service	HC+H2+H2S+H2O		HC+H2+H2S+H2O		N2
7	Heat Absorption, kW	9390 (13)		4370		700 (14)
8	Fluid					
9	Flow Rate, kg/hr	212924 (12)		78191 (12)		14975
10	Turndown Max.					
11	Pressure Drop, Allowable (Clean/Fouled), bar	1.0		1.0		(23)
12	Pressure Drop, Calculated (Clean / Fouled), bar					
13	Avg. Rad. Sect. Flux Density, Allowable, W/m2	37800 (16)		37800 (16)		A1
14	Avg. Rad. Sect. Flux Density, Calculated, W/m2					
15	Max. Rad. Sect. Flux Density, W/m2					
16	Conv. Sect. Flux Density (Bare Tube), W/m2					
17	Velocity Limitation, m/sec					
18	Process Fluid Mass Velocity, kg/sec-m2					
19	Max. Allow. / Calc. Inside Film Temp., °C					
20	Fouling Factor, m2-°K/W	0.00035		0.00035		
21	Coking Allowance, mm					
22	INLET CONDITIONS :					
23	Temperature, °C	326		268		30
24	Pressure, barA	20.8		19.3		7.1
25	Liquid Flow, kg/hr					
26	Vapor Flow, kg/hr	212924		78191		14975
27	Liquid Gravity, (Deg. API) (Sp. Gr.@15 °C)					
28	Vapor Molecular Weight	43.5		35.3		28
29	Viscosity, (Liquid / Vapor), mPaS	0.019		0.019		0.017
30	Specific Heat, (Liquid / Vapor), kJ/kg-K	2.844		3.178		1.053
31	Thermal Conductivity, (Liquid / Vapor), W/m-K	0.105		0.122		0.026
32	OUTLET CONDITIONS :					
33	Temperature, °C	380 (15)		330		200
34	Pressure, barA	(19)		(19)		(23)
35	Liquid Flow, kg/hr					
36	Vapor Flow, kg/hr	212924		78191		14975
37	Liquid Gravity, (Deg. API) (Sp. Gr.@15 °C)					
38	Vapor Molecular Weight	43.5		35.3		28
39	Viscosity, (Liquid / Vapor), mPaS	0.020		0.021		0.025
40	Specific Heat, (Liquid / Vapor), kJ/kg-K	2.985		3.344		1.077
41	Thermal Conductivity, (Liquid / Vapor), W/m-K	0.122		0.144		0.037
42	REMARKS AND SPECIAL REQUIREMENTS :					
43	Distillation Data or Feed Composition :					
44	Short Term Operating Conditions :					
45						
46	NOTES :					
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					CLASS 2
		PROCESS DATA SHEET FOR HDS REACTOR HEATER (H-8201) OF RFCC NAPHTHA TREATING UNIT			PAGE 4 OF 14
1	Type of Heater	<i>Cylindrical</i>	Manufacturer		Rev
2	Total Heater Absorbed Duty, MW	11.03 (13)			
3	PROCESS DESIGN CONDITIONS				
4	Operating Case	Max case polish burning	Max case polish burning	Sulfiding Case	A1
5	Heater Section	<i>Radiant & Conv.</i>	<i>Radiant & Conv.</i>	<i>Radiant & Conv.</i>	A1
6	Service	<i>MP Steam + Air(3% O2)</i>	<i>MP Steam + Air(8% O2)</i>	H2+H2S (31)	A1
7	Heat Absorption, kW	13103(30)	13068	3552	A1
8	Fluid				
9	Flow Rate, kg/hr	90842	90842	16923	A1
10	Turndown Max.				
11	Pressure Drop, Allowable (Clean/Fouled), bar	(23)	(23)	(23)	A1
12	Pressure Drop, Calculated (Clean / Fouled), bar				
13	Avg. Rad. Sect. Flux Density, Allowable, W/m2				
14	Avg. Rad. Sect. Flux Density, Calculated, W/m2				
15	Max. Rad. Sect. Flux Density, W/m2				
16	Conv. Sect. Flux Density (Bare Tube), W/m2				
17	Velocity Limitation, m/sec				
18	Process Fluid Mass Velocity, kg/sec-m2				
19	Max. Allow. / Calc. Inside Film Temp., °C				
20	Fouling Factor, m2-K/W				
21	Coking Allowance, mm				
22	INLET CONDITIONS :				
23	Temperature, °C	214	171	198	A1
24	Pressure, barA			17.87 (33)	A1
25	Liquid Flow, kg/hr				
26	Vapor Flow, kg/hr	90842	90842	16923	A1
27	Liquid Gravity, (Deg. API) (Sp. Gr.@15 °C)				
28	Vapor Molecular Weight	19.58	22.18	5.6	A1
29	Viscosity, (Liquid / Vapor), mPaS	0.018	0.019	0.012	A1
30	Specific Heat, (Liquid / Vapor), kJ/kg-K	1.92	1.61	6.323	A1
31	Thermal Conductivity, (Liquid / Vapor), W/m-K	0.036	0.033	0.206	A1
32	OUTLET CONDITIONS :				
33	Temperature, °C	490 (15)	500 (15)	315	A1
34	Pressure, barA	(23)		(23)	
35	Liquid Flow, kg/hr				
36	Vapor Flow, kg/hr	90842	90842	16923	A1
37	Liquid Gravity, (Deg. API) (Sp. Gr.@15 °C)				
38	Vapor Molecular Weight	19.58	22.18	5.6	A1
39	Viscosity, (Liquid / Vapor), mPaS	0.029	0.031	0.015	A1
40	Specific Heat, (Liquid / Vapor), kJ/kg-K	1.92	1.62	6.595	A1
41	Thermal Conductivity, (Liquid / Vapor), W/m-K	0.064	0.058	0.246	A1
42	REMARKS AND SPECIAL REQUIREMENTS :				
43	Distillation Data or Feed Composition :				
44	Short Term Operating Conditions :				
45					
46	NOTES :				
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COMBUSTION DESIGN CONDITIONS										Rev	
1											
2	Operating Case	10 PPM EOR									
3	Type of Fuel	Fuel Gas									
4	Excess Air, %	15%									
5	Calculated Heat Release (LHV), KW										
6	Fuel Efficiency Calculated, % (LHV)										
7	Fuel Efficiency Guaranteed, % (LHV)	78									
8	Radiation Loss, Percent of Heat Release (LHV)	1.5%									
9	Flue Gas Temp. Leaving :	Radiant Sect., °C									
10		Convection Sect., °C									
11		Air Preheater, °C									
12	Flue Gas Quantity, kg/hr										
13	Flue Gas Mass Velocity through Conv. Sect., kg/sec-m2										
14	Draft :	at Arch, mm H2O									
15		at Burners, mm H2O									
16	Ambient Air Temp., Efficiency Calculation, °C	25									
17	Ambient Air Temp., Stack Design, °C										
18	Altitude Above Sea Level, mm										
19	Volumetric Heat Release (LHV), kcal/hr-m3										
20	FUEL CHARACTERISTICS										
21	LIQUID TYPE			GAS TYPE			OTHER TYPE				
22	Heating Value LHV	kcal/kg	Heating Value LHV	35.4 (32)	MJ/Nm3	Heating Value LHV	kcal/kg			A1	
23	HHV	kcal/kg	HHV		MJ/Nm3	HHV	kcal/kg				
24	Press. @Burner	barG	Press. @Burner		barG	Press. @Burner	barG				
25	Temp. @Burner	°C	Temp. @Burner		°C	Temp. @Burner	°C				
26	Viscosity @	°C	SSU	Molecular Weight		Molecular Weight					
27	Atomizing Steam Temp.	°C									
28	Pressure	kg/cm2G									
29	COMPOSITION	WT % (Liquid)	COMPOSITION	VOL % (Gas)	COMPOSITION						
30	Sp.Gr / API Degree		Methane	83.6~88.7							
31	H/C Ratio (by WT)		Ethane	3.7 - 8.8							
32	Sulfur		Propane	1.2 - 2.1							
33	Ash		N2	2.5 ~ 6.8							
34	Nitrogen		n-Butane	Trace~0.5							
35	Metals		i-Butane	0.2 - 1.3							
36	- V (ppm)		n-Pentane	Nil ~ 0.1							
37	- Fe (ppm)		i-Pentane	Nil ~ 0.2							
38	- Ni (ppm)		H2S	Trace							
39	- Na (ppm)		RHS	Trace							
40											
41	BURNER DATA										
42	Manufacturer :	Size / Model :			Number :						
43	Type :	Location :			Orientation :						
44	Heat Release per Burner, 10 ⁶ kcal/hr	Design :			Normal :			Minimum			
45	Pressure Drop Across Burner @Design Heat Release, mm H2O :										
46	Distance Burner Center Line to Tube Center Line, mm	Horizontal :			Vertical :						
47	Distance Burner Center Line to Unshielded Refractory, mm	Horizontal :			Vertical :						
48	Pilot , Type :	Capacity, 10 ⁶ kcal/hr :									
49	Ignition Method :										
50	Design Fuel Rate, Guranteed, kg/hr :										
51	Flame Scanners, Location :	Number :									
52	Required Emissions : ppmv(d) (Corrected to 3% O2)	NOx :			CO :						
53	kg/kcal (LHV) (HHV)	UHC :			Particulates :						
54	NOTES :										
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		CON. NO.: ۷۳-۰۱-۲۰۰۱ پ پ س ص		CLASS 2		
		PROCESS DATA SHEET FOR HDS REACTOR HEATER (H-8201) OF RFCC NAPHTHA TREATING UNIT		PAGE 6 OF 14		
1	MECHANICAL DESIGN CONDITIONS					Rev
2	Plot Limitations :	Stack Limitations :				
3	Tube Limitations :	Noise Limitations :				
4	Structural Design Data :	Wind Velocity :	33.34m/s	Wind Occurence :		
5		Snow Load :	150kg/sq.m.	Seismic Zone :		
6	Min. / Nor. / Max. Ambient Air Temp., °C :	Relative Humidity, % :				
7	Heater Section :	Convention		Radiant Chamber		
8	Service :	Process		Process		
9	COIL DESIGN :					
10	Design Basis : Tube Wall Thick. (Code or Spec.)	API 530		API 530		
11	Rupture Strength (Min. or Avg.)					
12	Design Life, hr					
13	Design Pressure, Elastic / Rupture, barG					
14	Design Fluid Temp., °C					
15	Temperature Allowance, °C					
16	Corrosion Allowance, Tubes / Fittings, mm	3	3	3	3	
17	Hydrostatic Test Pressure, barG					
18	Post Weld Heat Treatment (Yes or No)	As per code		As per code		
19	Percent of Welds Fully Radiographed					
20	Maximum (Clean) Tube Metal Temperature, °C					
21	Design Tube Metal Temperature, °C					
22	Inside Film Coefficient, kcal/hr-m ² -°C					
23	COIL ARRANGEMENT :					
24	Tube Orientation : Vertical or Horizontal					
25	Tube Material (ASTM Spec. and Grade)	SS 347H		SS 347H		
26	Tube Outside Diameter, mm					
27	Tube Wall Thickness, (Minimum) (Average), mm					
28	Number of Flow Passes					
29	Number of Tubes / Number of Tube Rows					
30	Number of Tubes per Row (Conv. Section)					
31	Overall Tube Length, mm					
32	Effective Tube Length, mm					
33	Bare Tubes : Number					
34	Total Exposed Surface, m ²					
35	Extended Surface Tubes : Number					
36	Total Exposed Surface, m ²					
37	Tubes Layout (In-Line or Staggered)					
38	Tube Spacing, Cent. To Cent. : Horizontal, mm					
39	Diagonal, mm					
40	Vertical, mm					
41	Spacing Tube Cent. To Furnace Wall, mm					
42	Corbels (Yes or No)					
43	Corbel Width, mm					
44	DESCRIPTION OF EXTENDED SURFACE :					
45	Type : (Studs) (Serrated Fins) (Solid Fins)					
46	Material	Stainless Steel		Stainless Steel		
47	Dimensions : Height, mm					
48	Thickness, mm					
49	Spacing (No./m)					
50	Maximum Tip Temperature (Calculated), °C					
51	Extension Ratio (Total Area / Bare Area)					
52	PLUG TYPE HEADERS :					
53	Type					
54	Material (ASTM Spec. and Grade)					
55	Nominal Rating					

		CON. NO.: ۳۳-۰۱-۲۰۰۱ / پی پ س ص		CLASS 2	
		PROCESS DATA SHEET FOR HDS REACTOR HEATER (H-8201) OF RFCC NAPHTHA TREATING UNIT		PAGE 7 OF 14	
1 MECHANICAL DESIGN CONDITIONS (Continued)					
2	Heater Section :	Convention		Radiant Chamber	
3	Service :	Process		Process	
4 RETURN BENDS :					
5	Type				
6	Material (ASTM Spec. and Grade)	SS 347H		SS 347H	
7	Nominal Rating or Schedule				
8	Location (F.B. = Fire Box / H.B. = Header Box)				
9 TERMINALS AND / OR MANIFOLDS :					
10	Type (BEV.=Beveled, MAN=Manifold, FLG.=Flanged)				
11	Inlet : Material (ASTM Spec. & Grade)	SS 347H		SS 347H	
12	Size	30"		30"	
13	Schedule or Thickness				
14	Number of Terminals				
15	Flange Material (ASTM Spec.& Grade)				
16	Flange Size & Rating	300#		300#	
17	Outlet : Material (ASTM Spec. & Grade)				
18	Size				
19	Schedule or Thickness				
20	Number of Terminals				
21	Flange Material (ASTM Spec.& Grade)				
22	Flange Size & Rating	300#		300#	
23	Manifold to Tube Connection (Welded, Extruded, etc)				
24	Manifold Location (Inside or Outside Header Box)				
25 CROSSOVERS :					
26	Welded or Flanged				
27	Pipe Material (ASTM Spec. and Grade)	SS 347H			
28	Pipe Size				
29	Schedule or Thickness				
30	Flange Material				
31	Flange Size / Rating				
32	Location (Internal / External)				
33	Fluid Temp., °C				
34 TUBE SUPPORTS :					
35	Location (Ends / Top / Bottom)				
36	Material (ASTM Spec. and Grade)				
37	Design Metal Temp., °C				
38	Thickness, mm				
39	Insulation : Thickness, mm	(5)			
40	Material				
41	Anchor (Material and Type)				
42 INTERMEDIATE TUBE SUPPORTS :					
43	Material (ASTM Spec. and Grade)				
44	Design Metal Temp., °C				
45	Thickness, mm				
46	Spacing, mm				
47 TUBE GUIDES :					
48	Location				
49	Material				
50	Type / Spacing				
51 HEADER BOXES :					
52	Location :	Hinged Door / Bolted Panel :			
53	Casing Material :	Thickness, mm :			
54	Lining Material :	Thickness, mm :			
55	Anchor (Material and Type) :				

		CON. NO.: ۷۲-۰۱-۲۰۰۱ / پ پ س ص		CLASS 2
		PROCESS DATA SHEET FOR HDS REACTOR HEATER (H-8201) OF RFCC NAPHTHA TREATING UNIT		PAGE 8 OF 14
1	MECHANICAL DESIGN CONDITIONS (Continued)			Rev
2	REFRACTORY DESIGN BASIS :			
3	Ambient, °C :	Wind Velocity, m/sec :	Casing Temp., °C :	
4	EXPOSED VERTICAL WALLS :			
5	Lining Thickness, mm :	Hot Face Temp. : Service, °C :	Calculated, °C	
6	Wall Construction :			
7				
8	Anchor (Material & Type) :			
9	Casing Material :	Thickness, mm :	Temp., °C :	
10	SHIELDED VERTICAL WALLS :			
11	Lining Thickness, mm :	Hot Face Temp. : Service, °C :	Calculated, °C	
12	Wall Construction :			
13				
14	Anchor (Material & Type) :			
15	Casing Material :	Thickness, mm :	Temp., °C :	
16	ARCH :			
17	Lining Thickness, mm :	Hot Face Temp. : Service, °C :	Calculated, °C	
18	Wall Construction :			
19				
20	Anchor (Material & Type) :			
21	Casing Material :	Thickness, mm :	Temp., °C :	
22	FLOOR :			
23	Lining Thickness, mm :	Hot Face Temp. : Service, °C :	Calculated, °C	
24	Floor Construction :			
25				
26	Casing Material :	Thickness, mm :	Temp., °C :	
27	Minimum Floor Elevation, mm :	Free Space Below Plenum, mm :		
28	CONVECTION SECTION :			
29	Lining Thickness, mm :	Hot Face Temp. : Service, °C :	Calculated, °C	
30	Wall Construction :			
31				
32	Anchor (Material & Type) :			
33	Casing Material :	Thickness, mm :	Temp., °C :	
34	INTERNAL WALL :			
35	Type :	Material :		
36	Dimension, Height / Width, mm :			
37	DUCTS :	FLUE GAS	COMBUSTION AIR	
38	Location	Breeching		
39	Size, m or Net Free Area, m2			
40	Casing Material			
41	Casing Thickness, mm			
42	Lining : Internal / External			
43	Thickness, mm			
44	Material			
45	Anchor (Material & Type)			
46	Casing Temp., °C			
47	PLENUM CHAMBER (AIR) :			
48	Type of Plenum (Common or Integral) :			
49	Casing Material :	Thickness, mm :	Size mm :	
50	Lining Material :	Thickness, mm :		
51	Anchor (Material & Type) :			
52	NOTES :			
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1	MECHANICAL DESIGN CONDITIONS (Continued)					Rev
2	STACK OR STACK STUB :					
3	Number :	Self-Supported or Guyed	Location :			
4	Casing Material :	Thickness, mm :	Minimum Thickness, mm :			
5	Inside Metal Dia., mm :	Height Above Grade, m :	Stack Length, mm :			
6	Lining Material :	Thickness, mm :				
7	Anchor (Material & Type) :					
8	Extent of Lining :		Internal or External :			
9	Design Flue Gas Velocity, m/sec :		Flue Gas Temp., °C :			
10	DAMPERS :					
11	Location					
12	Type (Control / Tight Shut-off / etc.)					
13	Material : Blade					
14	Shaft					
15	Multiple / Single Leaf					
16	Provision for Operation (Manual or Automatic)					
17	Type of Operator (Cable or Pneumatic)					
18	PLATFORMS :					
19	Location	Number	Width, mm	Length / Arc	Stairs / Ladder	Access From
22						
23						
24						
25	Type of Flooring :					
26	DOORS :					
27	Type	Number	Location	Size, mm	Bolted / Hinged	
28	Access					
29	Explosion					
30	Observation					
31	Tube Removal					
32	MISCELLANEOUS :					
33	Instrument Connections :		Number	Size, mm	Type	
34	Process Fluid	Temperature, Cross over and Radiant outlet				
35	Pressure					
36	Blank-off					
37	Combustion Air	Temperature				
38	Pressure					
39	Flue Gas	Temperature, Below conv.section & above damper				
40	Pressure					
41	Draft Connections (10)					
42	Flue Gas Sample					
43	Snuffing Steam / Purge , Radiant floor. Conv. And header boxes					
44	O2 Analyzer, Below conv.section & below damper					
45	CO / NOx Analyzer					
46	Vents / Drains					
47	EPA Connections					
48	Tube Skin Thermocouples, Radiant wall.Steam coil and lowest shield row					
49	Flame Scanner					
50	Painting Requirements :					
51	Internal Coating :					
52	Galvanizing Requirements :					
53	Are Painters Trolley and Rail Included (Yes or No) :					
54	Special Equipment :	Sootblowers :				
55	Air Preheater :					

1	GENERAL DATA		Rev
2	Type of Heater	<i>Cylindrical</i>	
3	Altitude Above Sea Level, mm		
4	Air Supply :		
5	Ambient / Preheated Air / Gas Turbine Exhaust		
6	Temperature, °C (Min. / Max. / Design)		
7	Relative Humidity, %		
8	Draft Type : Forced / Natural / Induced		
9	Draft Available : Across Burner, mm H ₂ O		
10	Across Plenum, mm H ₂ O		
11	Required Turndown		
12	Burner Wall Setting Thickness, mm		
13	Heater Casing Thickness, mm		
14	Firebox Height, mm		
15	Tube Circle Diameter, mm		
16	BURNER DATA		
17	Manufacturer		
18	Type of Burner	Natural Draft - Low Noise and Ultra Low Nox	
19	Model / Size		
20	Direction of Firing		
21	Location (Roof / Floor / Sidewall)		
22	Number Required (23, 24)		
23	Minimum Distance Burner Centerline, mm		
24	to Tube Centerline (Horizontal / Vertical)		
25	to Adjacent Burner Centerline (Horizontal / Vertical)		
26	to Unshielded Refractory (Horizontal / Vertical)		
27	Burner Circle Diameter, mm		
28	Pilots :		
29	Number Required		
30	Type		
31	Ignition Method		
32	Fuel		
33	Fuel Pressure, barG		
34	Capacity, 10 ⁶ kcal/hr		
35	OPERATING DATA		
36	Fuel		
37	Heat Release per Burner, 10 ⁶ kcal/hr (LHV)		
38	Design		
39	Normal		
40	Minimum		
41	Excess Air @ Design Heat Release, %		
42	Air Temperature, °C		
43	Draft (Air Pressure) Loss, mmH ₂ O		
44	Design		
45	Normal		
46	Minimum		
47	Fuel Pressure Required @ Burner, barG		
48	Flame Length @ Design Heat Release, mm		
49	Flame Shape (Round, Flat, etc)		
50	Atomizing Medium / Oil Ratio, kg/kg		
51	NOTES :		
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1		GAS FUEL CHARACTERISTICS			Rev
2	Fuel Type	Fuel Gas			
3	Heating Value (LHV), MJ/Nm3	35.4 (32)			
4	Specific Gravity (Air=1.0)				
5	Molecular Weight				
6	Fuel Temperature @ Burner, °C	21.06			
7	Fuel Pressure; Available @ Burner, barG	2.8 (25)			
8	Fuel Gas Composition, Vol%				
9	CH4	83.6-88.7			
10	C2H6	3.7 - 8.8			
11	C3H8	1.2 - 2.1			
12	n-C4H10	Trace ~ 0.5			
13	i-C4H10	0.2 - 1.3			
14	n-C5H12	Nil ~ 0.1			
15	i-C5H12	Nil ~ 0.2			
16	H2S	Trace			
17					
18	N2	2.5 - 6.8			
19	RHS	Trace			
20	Total	100			
21					
22					
23					
24	LIQUID FUEL CHARACTERISTICS				
25	Fuel Type				
26	Heating Value (LHV), kcal/kg				
27	Specific Gravity / Degree API				
28	H / C Ratio (by Weight)				
29	Viscosity, @ °C, SSU				
30	@ °C, SSU				
31	Vanadium, ppm				
32	Sodium, ppm				
33	Potassium, ppm				
34	Nikel, ppm				
35	Fixed Nitrogen, ppm				
36	Sulfur, %wt				
37	Ash, %wt				
38	Liquids : ASTM Initial Boiling Point, °C				
39	ASTM End Point, °C				
40	Fuel Temperature @ Burner, °C				
41	Fuel Pressure; Available / Required @ Burner, barG				
42	Atomizing Medium Air / Steam / Mechanical				
43	Temperature, °C				
44	Pressure, barG				
45	NOTES :				
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1		MISCELLANEOUS				Rev
2	Burner Plenum :	Common / Integral				
3		Material				
4		Plate Thickness, mm				
5		Internal Insulation				
6	Inlet Air Control :	Damper or Registers				
7		Mode of Operation				
8		Leackage, %				
9	Burner Tile :	Composition				
10		Minimum Service Temperature, °C				
11	Noise Specification					
12	Attenuation Method					
13	Painting Requirements					
14	Ignition Port :	Size / No.				
15	Sight Port :	Size / No.				
16	Flame Detection :	Type	UV Scanner			
17		Number / Location				
18		Connection Size				
19	Safety Interlock System for Atomizing Medium & Oil					
20	Performance Test Required (Yes or No)					
21	EMISSION REQUIREMENTS- Dry Flue Gas at 3 % O2 (17)					
22	Firebox Temperature, °C					
23	Nox		432 mg/Nm3, 210 ppmv			
24	CO		130 ppmv			
25	UHC					
26	Particulates		50 mg/Nm3			
27	Sox		800 ppmv			
28						
29	* Corrected to 3% O2 (Dry Basis @ Design Heat Release)					
30	NOTES :					
31	1. At design conditions, minimum of 90% of the available draft with air register fully open shall be utilized across the burner.					
32	In addition, a minimum of 75% of the air side pressure drop with air registers full open shall be utilized across burner throat.					
33	2. Vendor to guarantee burner flame length.					
34	3. Vendor to guarantee excess air, heat release and draft loss across burner.					
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36						
37						
38						
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NOTES

1	(1) Dampers are to be failure open. Dampers shall be provided with external position indicator and transmitter to indicate	Rev																					
2	positions in the control room. Damper bearing shall be located external to casing. Manual override to be provided.																						
3	(2) Tube wall thickness shall be calculated in accordance with API530.																						
4	(3) Design temp. for calculating tube wall thickness shall be 27 °C above the max. calculated tube wall temperature.																						
5	(4) End tubesheet shall be insulated on the hot side and shall equipped with 18/8 Cr/Ni sleeves to protect insulation from																						
6	damaged by tubes																						
7	(5) Min. end tubesheet thickness shall be 12.5mm and intermediate tubesheets 16mm.																						
8	(6) Header boxes and firebox shall be provided with a 2" flanged connections c/w blinds for snuffing steam connections.																						
9	(7) Inspection doors shall be provided to permit 100% observation of radiant tubes, including convection tubes exposed to radiant heat.																						
10	(8) Peep holes shall be located so that the burner flames can be adjusted while observing burners.																						
11	(9) Provide max possible access door in arch for tube removal and 600mm x600mm access door in radiant floor.																						
12	(10) The Flue gas Pressure gauges shall be located at burners, below convection section, below and above stack damper.	A1																					
14	(11) Provide 2.5mm thick erosion resistant stainless steel shroud in place for future sootblower lane.																						
15	(12) Design flowrate: 256976 kg/hr (120.7 % of 10 ppm SOR flowrate). Turndown flowrate during regeneration: 5.4 % of normal flowrate	A1																					
16	(11477 kg/hr corresponding of burning phase during catalyst HR-845 regeneration). Turndown flowrate in normal operation: 54 %																						
17	of normal flowrate (corresponding of turndown of 50 ppm SOR run case).																						
18	(13) Design Duty 11.03 MW (absorbed)																						
19	(14) Turndown value during regeneration (corresponding of heating phase during catalyst HR-841 regeneration).																						
20	(15) <i>Design values of piping for normal/regeneration cases are given.</i>																						
21	<i>Normal Inlet : 26.0/FV (at ambient) barg @ 350 °C, Normal Outlet : 26.0/FV (at ambient) barg @ 405 °C</i>																						
	<i>Regeneration outlet : 8.0 barg @ 525 °C.</i>	A1																					
22	Steam-out: Operating conditions is 190°C at ATM, and its design conditions is 265°C at ATM.	A1																					
	Full Vacuum @ 212 °C (MP steam saturation temperature)																						
23	<table border="1"> <thead> <tr> <th>Operation</th> <th>Fluid Composition</th> <th>P inlet in barg</th> <th>T inlet °C</th> <th>T outlet</th> <th>Mw</th> <th>State</th> </tr> </thead> <tbody> <tr> <td>Sulfiding</td> <td>H2 + H2S</td> <td>17.05</td> <td>198</td> <td>315</td> <td>5.6</td> <td>V</td> </tr> <tr> <td>Regeneration</td> <td>N2 + CO2 + O2+ H2O</td> <td>6.3</td> <td>260</td> <td>500</td> <td>18</td> <td>V</td> </tr> </tbody> </table>	Operation	Fluid Composition	P inlet in barg	T inlet °C	T outlet	Mw	State	Sulfiding	H2 + H2S	17.05	198	315	5.6	V	Regeneration	N2 + CO2 + O2+ H2O	6.3	260	500	18	V	
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Regeneration	N2 + CO2 + O2+ H2O	6.3	260	500	18	V																	
24																							
25																							
26	(16) Max. allowable heat flux for single firing heater: 37.8 kW/m2																						
27	Max. allowable heat flux for double firing heater: 58.6 kW/m2																						
28	(17) According to EPPC Standard																						
29	(18) Header will also receive polluted air from Merox Unit (25 kg/hr, 0.05 barg (will be finalized later) , 46 °C) for combustion in the firebox. The	A1																					
30	contain ~ 88.5 vol.% N2 and 11.5 vol.% O2, as well as traces of mercaptans.																						
31	(19) Max. allowable pressure drop: 1 bar																						
32	(20) Max. continuous hydrogen partial pressure: 13.1 bar	Max. continuous hydrogen sulfide content: 0.04 mol%																					
33	During sulfiding procedure H2S content can be as high as 2 mol% during 12 hours every 3 years.																						
34	(21) Max. capacity of one burner shall not exceed 3 MW for design duty as per note 13																						
35	(22) MDMT : -15 °C																						
36	(23) Vendor to specify the allowable pressure drop for each case																						
37	(24) Combustion Air Condition																						
38	- Temperature : -15 / 41 degc (Min./Max.)																						
39	- Relative Humidity : 73 / 85 % (Average / Design)																						
40	- Altitude above sea level : 1685 m																						
41	(25) Fuel Gas B/L Pressure (will be finalized later) and vendor to provide required fuel gas pressure at burner.	A1																					
42	(26) Materials shall be specified in accordance with API 560.																						
43	(27) Hydrogen Service.																						
44	(28) for all instruments: Instrument specification and nozzle size shall meet the requirements of project specification:																						
45	JOB SPECIFICATION FOR INSTRUMENTATION Doc. No: "2001-00-ED-IN-SP-7001" and references standards.																						
46	(29) CEMS shall be considered by vendor.	A1																					
47	(30) Max. value during regeneration (corresponding of polish burning phase during catalyst HR-841 regeneration).	A1																					

NOTES

1			Rev
2	(31) <i>Fluid Composition in sulfiding case:</i>		A1
3		<i>%mol</i>	
4	<i>Hydrogen</i>	89.95	
5	<i>Water</i>	0	
6	<i>Nitrogen</i>	0	
7	<i>Carbon Dioxide</i>	0	
8	<i>Hydrogen Sulfide</i>	0.5	
9	<i>Methane</i>	2.89	
10	<i>Ethane</i>	2.69	
11	<i>Propane</i>	1.89	
12	<i>i-Butane</i>	1.79	
13	<i>Pentane</i>	0.7	
14			
15	(32) <i>As Fuel gas Composition is variable, LHV will be in range of 33.3~36.</i>		A1
16	(33) <i>Will be finalized later.</i>		
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